## THAT WHICH IS CLAIMED IS:

- 1. A method of hydrogenating a polymer, comprising the steps of:
- (a) providing a dense phase, said dense phase comprising a polymer in an organic solvent;
- (b) providing a catalyst system, said catalyst system comprising at least one metal hydrogenation catalyst selected from the group consisting of Nickel and Ruthenium immobilized on a solid support; and
- (c) providing a light phase, said light phase comprising hydrogen and carbon dioxide; and
- (d) contacting said dense phase, said light phase and said catalyst system so that said hydrogen reacts with said polymer and said polymer is hydrogenated.
- 2. The method of claim 1, wherein said polymer is selected from the group consisting of polystyrene, poly(bisphenol A carbonate), poly(ethylene terephthalate), polybutadiene and copolymers thereof, and polyisoprene and copolymers thereof.
- 3. The method of claim 1, wherein said solid support is formed from carbon, silica, alumina, silica-alumina, calcium carbonate or barium sulfate.
- 4. The method of claim 1, wherein said at least one metal hydrogenation catalyst further comprises a catalyst selected from the group consisting of platinum, palladium, rhodium, copper, molybdenum rhenium, tungsten, cobalt, and mixtures thereof
  - 5. The method of claim 1, wherein said metal hydrogenation catalyst is nickel.
- 6. The method of claim 1, wherein 0.1 to 1 weights of catalyst per weight of polymer are included in said contacting step.
- 7. The method of claim 1, wherein from 0.1 to 20 weight percent of said polymer is included in said dense phase.
- 8. The method of claim 1, wherein said contacting step is carried out at a carbon dioxide pressure of 100 to 3000 psi.

9. The method of claim 1, wherein said contacting step is carred out at a hydrogen pressure of 100 to 2000 psi.

- 10. The method of claim 1, wherein the viscosity of said dense phase at reaction temperature prior to said contacting step is from 1 to 100 centipoise, and wherein the viscosity of said dense phase after said contacting step decreased by at least half thereof.
- 11. The method of claim 1, wherein said light phase comprises a gas or supercritical fluid.
  - 12. The method of claim 1, wherein said dense phase comprises a liquid.
- 13. The method of claim 1, wherein said contacting step is carried out at a temperature of 0 to 300  $^{\circ}$ C.
- 14. The method of claim 1, wherein said contacting step is a batch contacting step.
- 15. The method of claim 1, wherein said contacting step is a continuous contacting step.
- 16. The method of claim 1, wherein said contacting step is carried out in slurry reactor.
- 17. The method of claim 1, wherein said contacting step is carried out in a fixed bed reactor.
- 18. The method of claim 1, wherein said contacting step is carried out in a fixed bed reactor selected from the group consisting of trickle bed reactors and two-phase upflow reactors.
  - 19. A method of hydrogenating a polymer, comprising the steps of:

(a) providing a liquid dense phase, said dense phase consisting essentially of a polymer in an organic solvent, said polymer selected from the group consisting of polystyrene, poly(bisphenol A carbonate), poly(ethylene terephthalate), polybutadiene and copolymers thereof, and polyisoprene and copolymers thereof, with said solvent included in said dense phase in an amount of from 0.1 to 20 weight percent;

- (b) providing a solid catalyst system, said catalyst system comprising at least one metal hydrogenation catalyst selected from the group consisting of nickel and ruthenium immobilized on a solid support; and
- (c) providing a gas or supercritical fluid a light phase, said light phase consisting essentially of hydrogen at a pressure of 100 to 2000 psi and carbon dioxide at a pressure of 100 to 3000 psi; and
- (d) contacting said dense phase, said light phase and said catalyst system at a temperature of 50 to 300 °C, and in an amount of 0.1 to 1 weight of catalyst system per weight of polymer, to react said hydrogen with said polymer hydrogen and hydrogenate said polymer.
- 20. The method of claim 19, wherein the viscosity of said dense phase prior at reaction temperature to said contacting step is from 1 to 100 centipoise, and wherein the viscosity of said dense phase after said contacting step is decreased by at least half thereof.
- 21. The method of claim 19, wherein said contacting step is a batch contacting step.
- 22. The method of claim 19, wherein said contacting step is a continuous contacting step.
- 23. The method of claim 19, wherein said contacting step is carried out in slurry reactor.
- 24. The method of claim 19, wherein said contacting step is carried out in a fixed bed reactor.

25. The method of claim 19, wherein said contacting step is carried out in a fixed bed reactor selected from the group consisting of trickle bed reactors and two-phase upflow reactors.

26. The method of claim 19, wherein said polymer is polystyrene, which polystyrene is hydrogenated to produce polycyclohexylethylene.